



# Development of Passive HC/NO<sub>x</sub> Trap Catalysts for Low Temperature Gasoline Applications

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Project ID #:  
ace130

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# Overview

## Timeline

- Project start date: 9/1/17
- Project end date: 8/31/20  
(now 11/30/20)
- Percent complete: 49%

## Budget

- Total project funding
  - DOE share: \$2,098,350
  - Contractor share: \$300,614
- Funding for FY 2018: \$845,015
- Funding for FY 2019: \$743,731

## Barriers and Technical Targets

- Barriers addressed:
  - Improve low temperature and cold start NOx control
  - Improve low temperature and cold start HC control
  - Characterize and understand Passive NOx Adsorber (PNA) durability

## Partners

- Collaboration: Ford, ORNL, Purdue, UC Berkeley, BASF
- Project lead: U. Kentucky

# Relevance

## Impact

- Improved Pd/zeolite HC/NO<sub>x</sub> adsorbers will enable vehicle manufacturers to satisfy future emission standards and improve vehicle fuel economy by reducing cold start fueling requirements

## Objectives

- Fundamental understanding of the chemistry of NO<sub>x</sub> adsorption and reduction in Pd/zeolites will be attained
- Pd/zeolites will be tailored with respect to performance and durability for application as HC/NO<sub>x</sub> adsorbers
- HC/NO<sub>x</sub> adsorber performance will be validated using exhaust gas from an engine dynamometer
- Scientific insights and technology will be transferred to the automotive industry via the project's industry partners

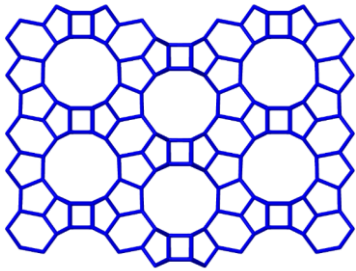
*While this technology should be applicable to both gasoline and diesel vehicles, gasoline applications are emphasized in this project, given the importance of stoichiometric engines in the U.S. automotive market*

# Milestones

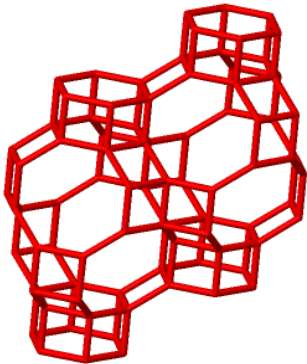
| Task                          | Date    | FY2018 Milestone Description   | Status        |
|-------------------------------|---------|--|---------------|
| Catalyst synthesis            | -       | Synthesis of large (10 g) batches of Pd/zeolites to distribute to the entire team as baseline catalysts  | Done          |
| Catalyst characterization     | 8/31/18 | Elucidation of the structure of Pd <sup>2+</sup> cations exchanged into CHA and BEA  | Done/on-going |
| Reactor studies<br>(Go/no-go) | -       | NO adsorption capacity of degreened Pd/CHA and Pd/BEA superior to Pd/CeO <sub>2</sub> -ZrO <sub>2</sub> benchmark in stoichiometric exhaust (<100 °C). | Done          |

| Task                             | Date     | FY2019 Milestone Description  | Status        |
|----------------------------------|----------|---|---------------|
| Spectroscopic studies            | 2/28/19  | Role of alkyl nitrite and isocyanate species in NO-C <sub>2</sub> H <sub>4</sub> and NO-CO co-adsorption delineated   | Done/on-going |
| Computational study              | 5/31/19  | Structure and IR spectra of NO, C <sub>2</sub> H <sub>4</sub> , and CH <sub>3</sub> C <sub>6</sub> H <sub>5</sub> adsorbed on Pd <sup>2+</sup> cations in CHA defined | Done/on-going |
| Computational study              | 8/31/19  | Structure and IR spectra of NO, C <sub>2</sub> H <sub>4</sub> , and CH <sub>3</sub> C <sub>6</sub> H <sub>5</sub> adsorbed on Pd <sup>2+</sup> cations in BEA defined | Done/on-going |
| Catalyst synthesis               | 11/30/19 | Baseline Pd-CHA and Pd-BEA monolith catalysts prepared  | To be done    |
| Catalyst synthesis<br>(Go/no-go) | 11/30/19 | Synthesis of Pd/zeolite catalyst (> 20 g) of optimized composition and structure  | To be done    |

# Approach



Beta (BEA)



Chabazite (CHA)

- Use combination of experimental and computational methods to allow a deeper understanding of the governing chemistry in Pd-zeolite PNAs
- Pd-CHA as (relatively!) simple system amenable to study, Pd-Beta as commercially relevant system
- Focus in Years 1 and 2 on understanding how framework type, SAR, Al distribution, etc., impact NO adsorption and desorption behavior
- Focus in Year 3 on design of optimized system and assessment of durability

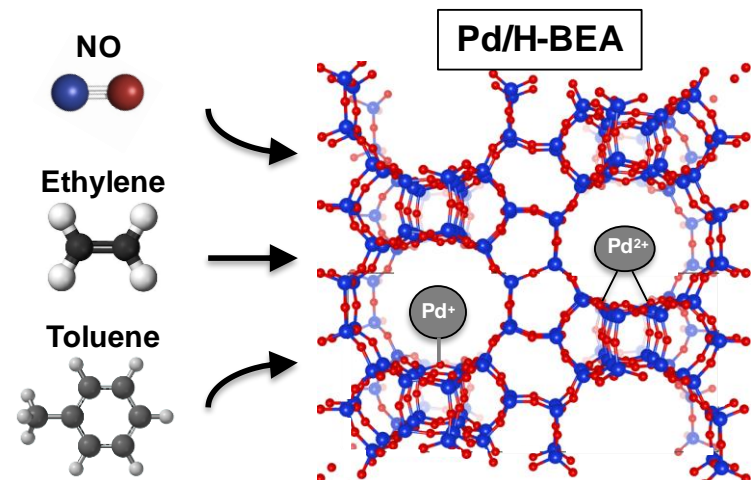
# Collaboration

- **UK** (Mark Crocker):  
Project management, spectroscopic studies (DRIFTS, ESR, XPS), catalyst aging
- **Purdue** (Raj Gounder):  
Zeolite/catalyst synthesis, catalyst characterization, spectroscopic studies (XAS)
- **UC Berkeley** (Alex Bell):  
NO<sub>x</sub>/HC adsorption/desorption and kinetic studies, computational studies
- **Ford** (Christine Lambert):  
NO<sub>x</sub>/HC adsorption/desorption studies, catalyst evaluation, emissions modeling
- **ORNL** (Vitaly Prikhodko):  
Catalyst characterization (TEM), catalyst aging, catalyst evaluation (slip stream from engine test bench)
- **BASF** (Xinyi Wei):  
Catalyst preparation (monoliths)

# Technical Accomplishments

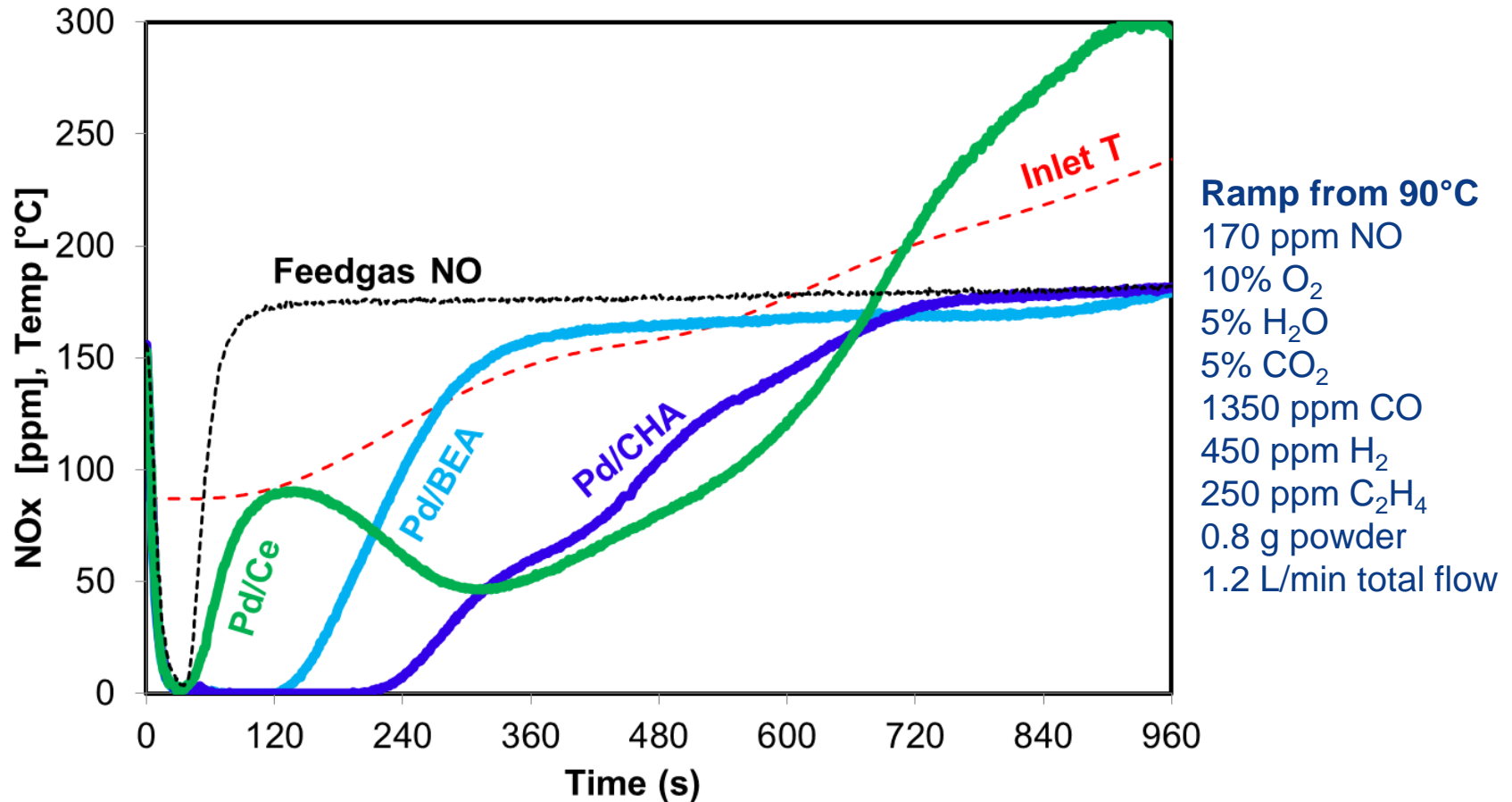
Work focused in five main areas to date:

- Pd-CHA and Pd-Beta synthesis and characterization
- Microreactor studies of NO adsorption and desorption
- Pd-CHA evaluation in simulated cold start tests
- DRIFTS studies to characterize Pd speciation and NO adsorption sites
- Computational studies to characterize Pd speciation and NO adsorption sites



# Comparing PNA Technologies (lean)

## Simulated cold start

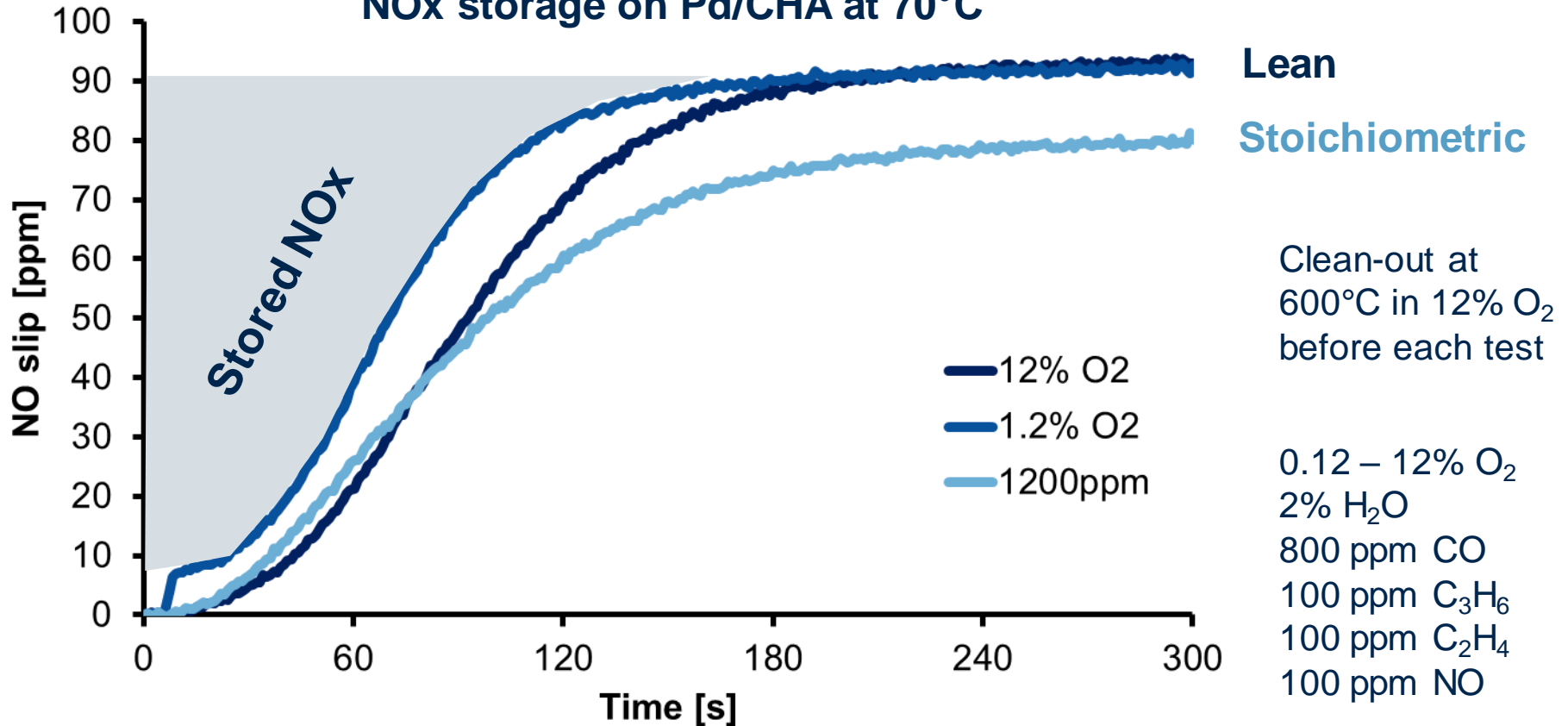


**Pd/CHA has higher storage efficiency than Pd/BEA or Pd/CeO<sub>x</sub>**



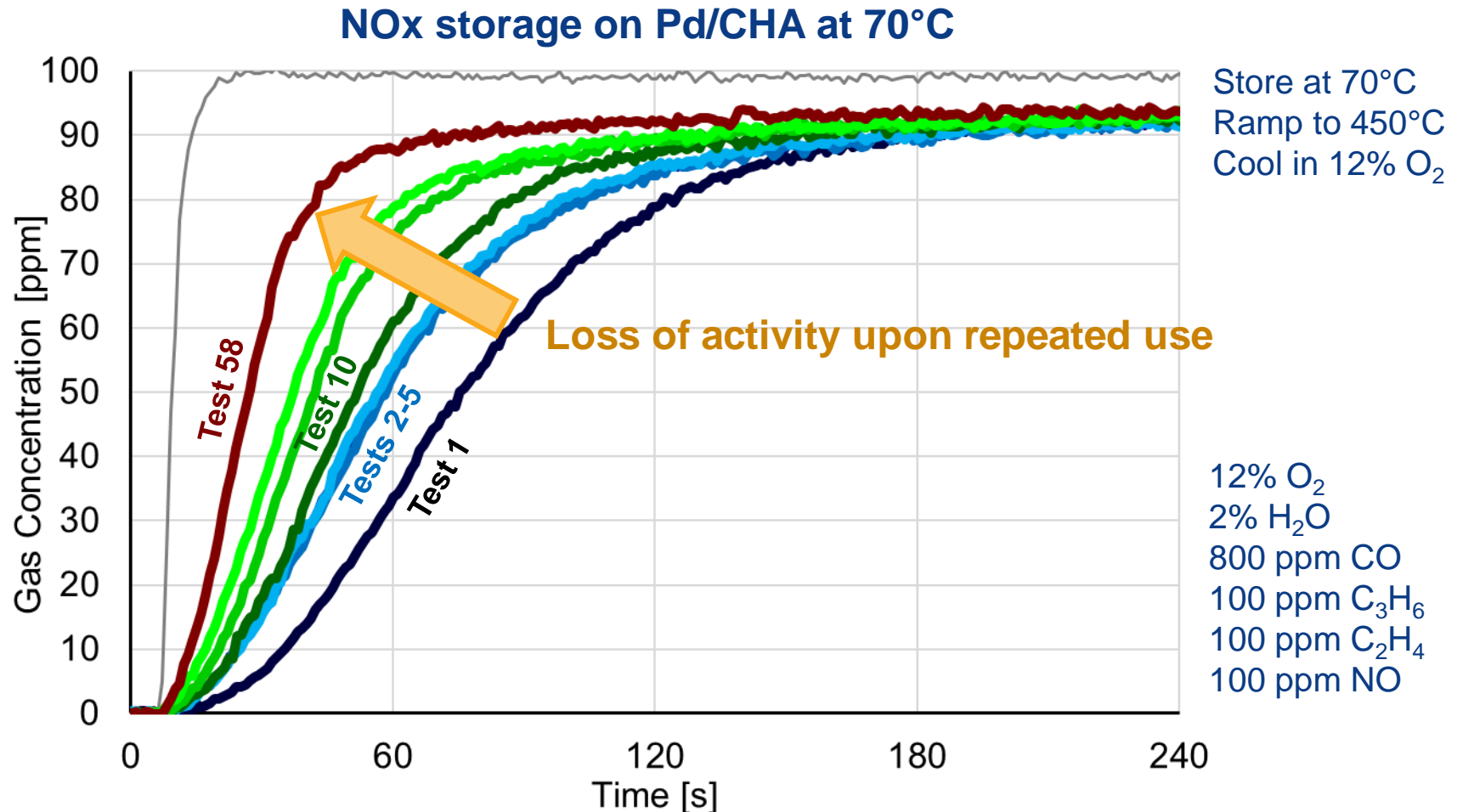
# From Lean to Stoichiometric Feed

NO<sub>x</sub> storage on Pd/CHA at 70°C



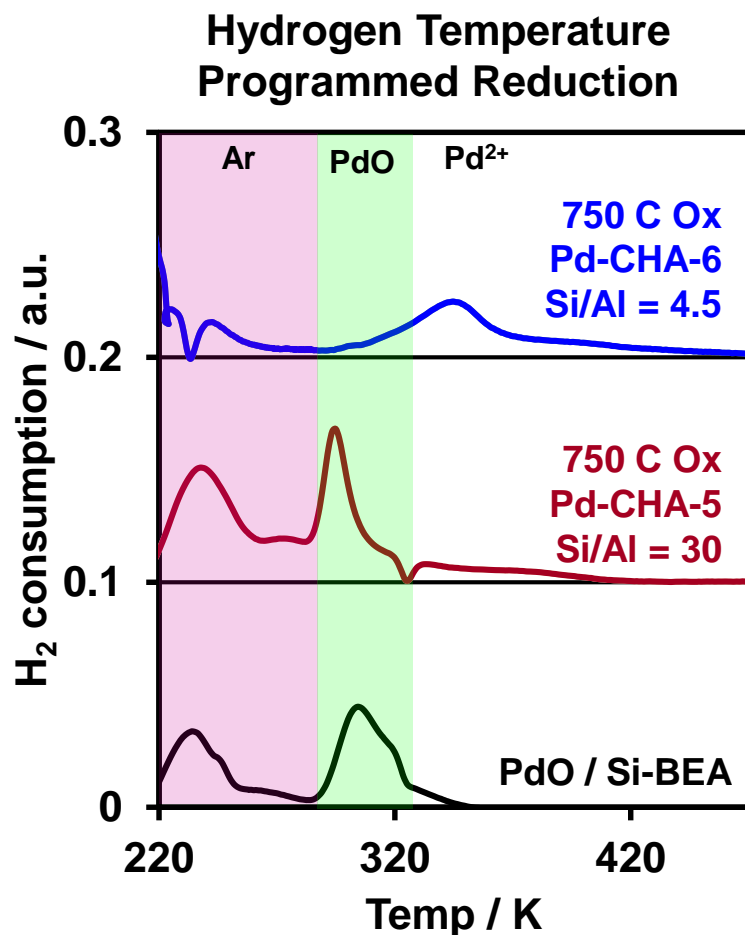
Oxygen level exerts only a relatively minor effect on NO<sub>x</sub> storage behavior

# Impact of Repeated Cycling

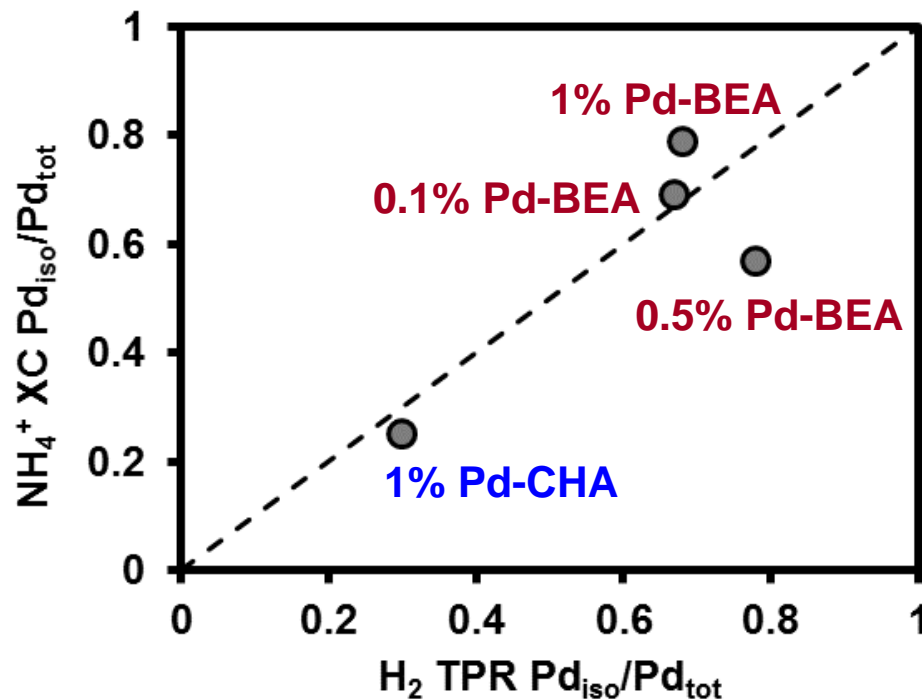


**Initially stable performance deteriorates substantially upon extended cycling; stability improvements are required for technology to be commercially viable**

# Characterization of Pd Species in Zeolites for PNA



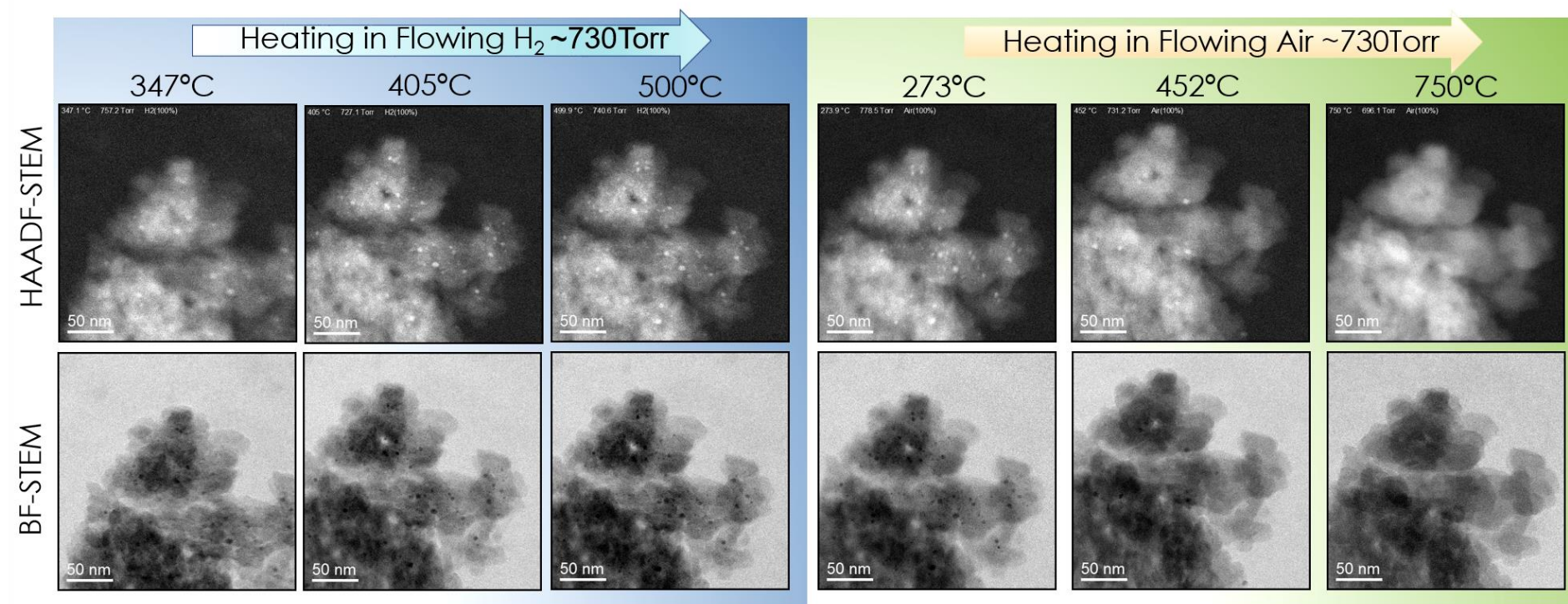
Parity plot comparing  $\text{NH}_4^+$  back exchange and  $\text{H}_2$  TPR quantifications (as-prepared state: 550 °C calcination)



- $\text{H}_2$  TPR can differentiate ion-exchanged Pd from PdO particles and investigate speciation after various in-situ pretreatments.
- $\text{NH}_4^+$  back exchange can selectively titrate ion-exchanged Pd
- In as-prepared state, Pd does not exchange into CHA as efficiently as for BEA

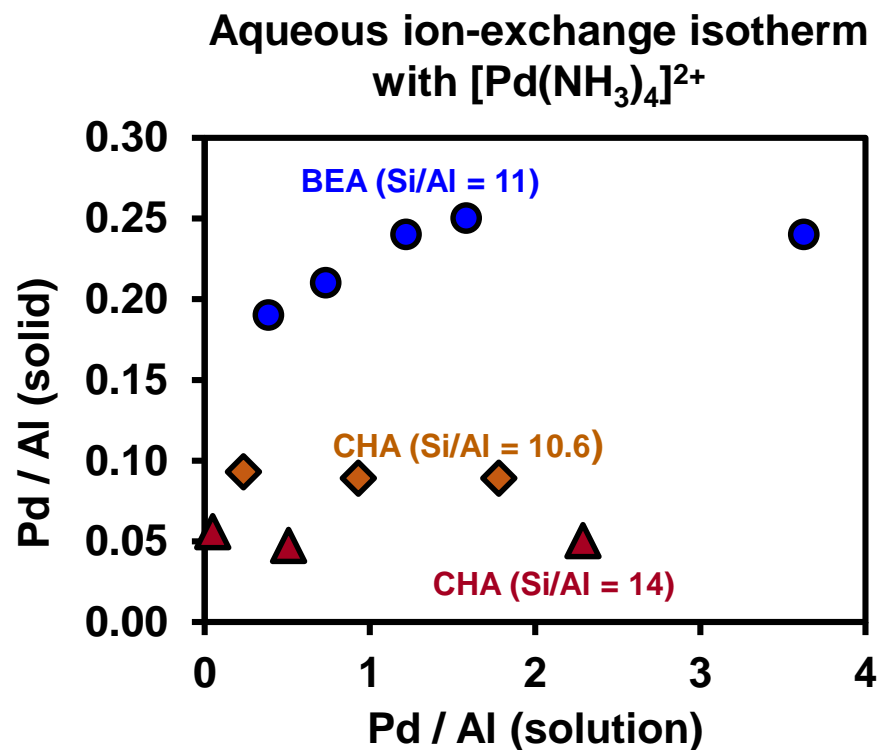
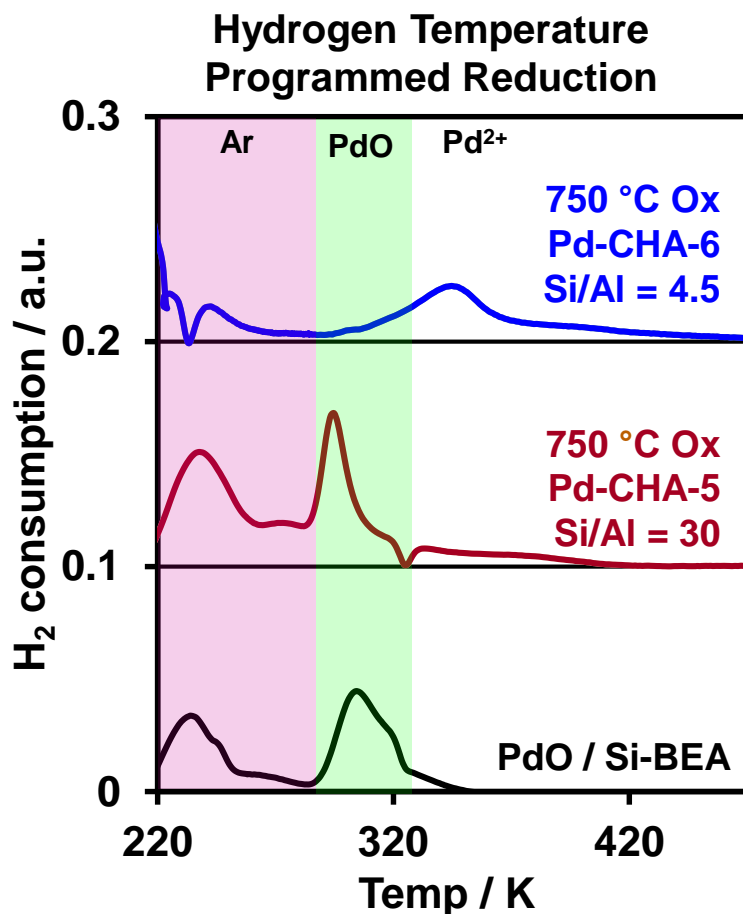
# In-situ STEM Characterization of Pd-BEA ( $\text{Pd}/\text{Al} = 0.09$ )

Ramp in  $\text{H}_2 \rightarrow$  Switch to  $\text{N}_2$  (20 Torr)  $\rightarrow$  Cool to room temp.  $\rightarrow$  Switch to air  $\rightarrow$  Start heating



- Increasing temperature in  $\text{H}_2$  generates more and larger Pd particles
- Dry air treatments at 452 °C (Tamman temp. = 240 °C) are able to re-oxidize and re-disperse Pd
- At 750 °C in dry air, the majority of the PdO particles have re-dispersed

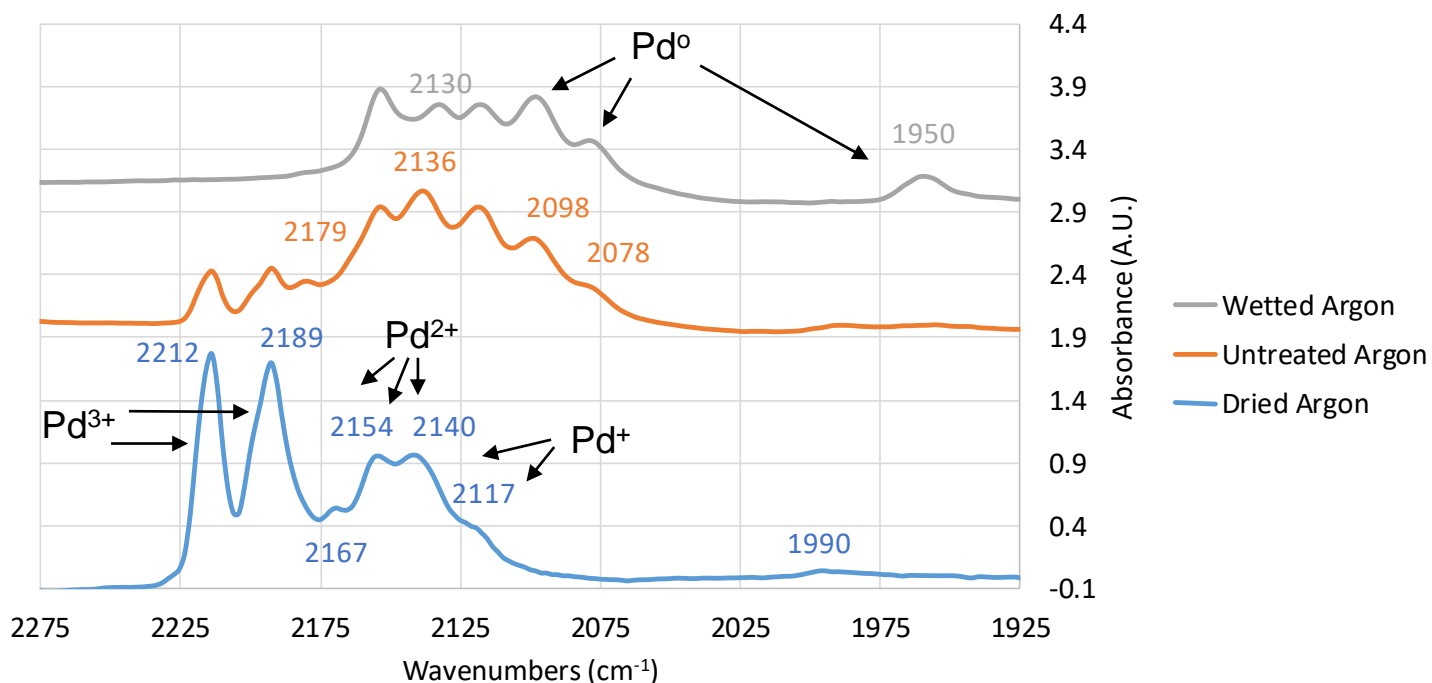
# Al Site Requirements to Stabilize Ion-exchanged Pd<sup>2+</sup>



- As the Al density increases, so do the number of sites capable of stabilizing ion-exchanged Pd<sup>2+</sup>
- Results suggest two, proximal Al sites are required for stabilizing ion-exchanged Pd<sup>2+</sup>
- Dry oxidation treatments are capable of yielding predominately ion-exchanged CHA
- Proposed stable Pd species on zeolites are PdO and Pd<sup>2+</sup> charge compensated by two Al sites

# DRIFTS: Effect of Water on Palladium Speciation

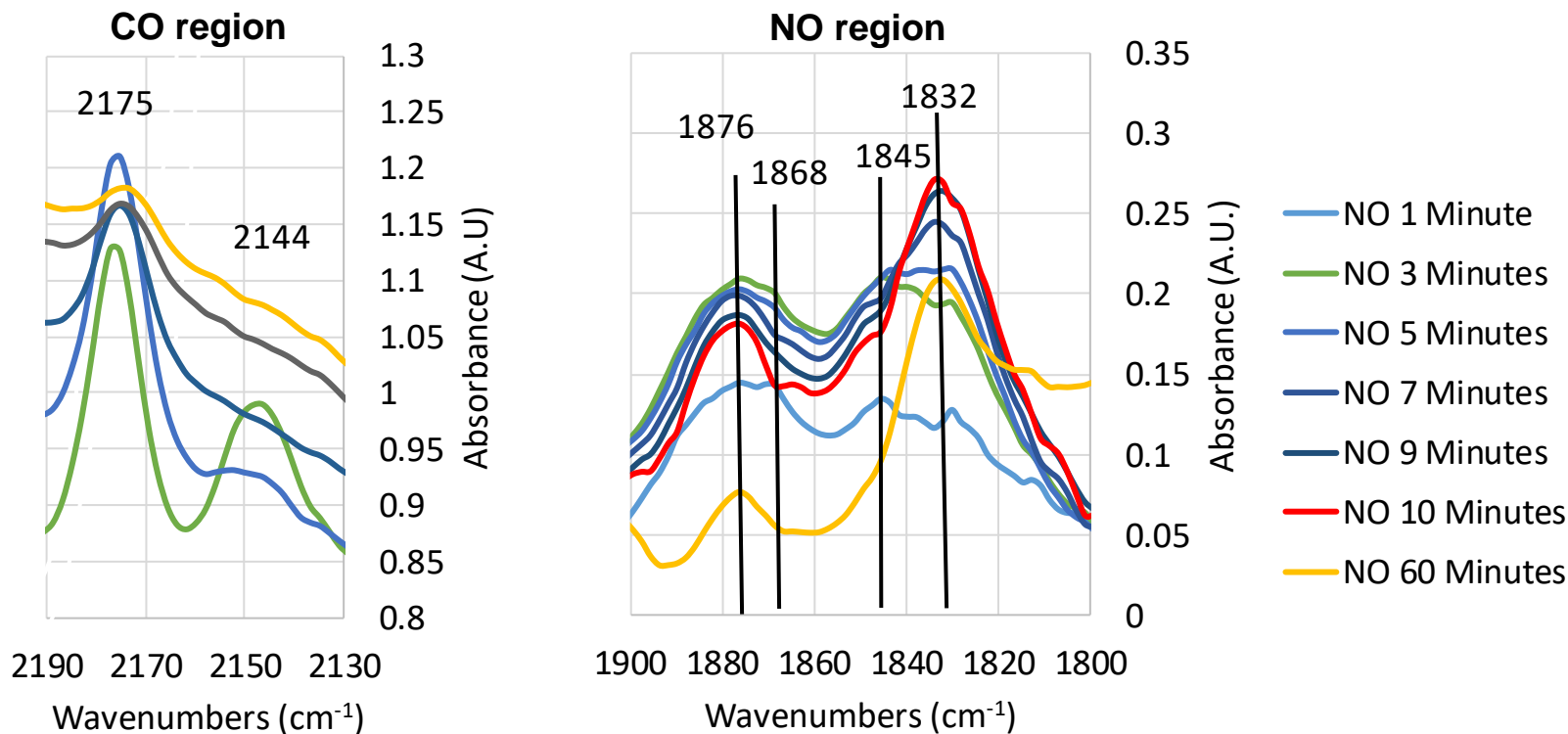
Pd-Beta treated in Ar at 500 °C, followed by CO adsorption at 25 °C



- Presence of trace amount of water (<5 ppm in untreated argon) acts to reduce palladium at high temperatures; increasing water concentration leads to more intense Pd<sup>0</sup>-CO bands (<2100 cm<sup>-1</sup>)
- Total elimination of trace water from the gas feed required to decouple effects of water from other gas species

# DRIFTS: CO Promotes NO Adsorption via Formation of $\text{Pd}(\text{CO})(\text{NO})^{n+}$ Complex

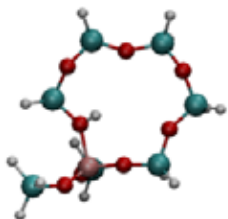
CO-NO Sequential Adsorption on Pd-Beta at 100 °C:



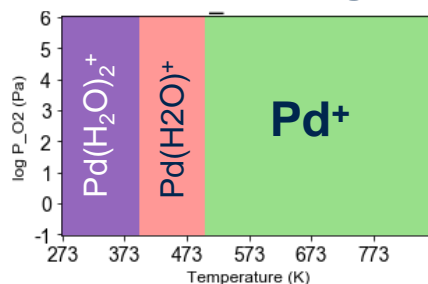
- $\text{Pd}(\text{CO})(\text{NO})^{n+}$  species identified at 1868, 1845  $\text{cm}^{-1}$  (N-O stretch) and 2175  $\text{cm}^{-1}$  (C-O stretch)
- Co-adsorption features increase in intensity until 3-5 minutes then decrease; after 60 minutes NO exposure, only NO remains adsorbed
- NO readily displaces CO from catalyst surface at 100 °C

# Pd Speciation in CHA by QMMM DFT

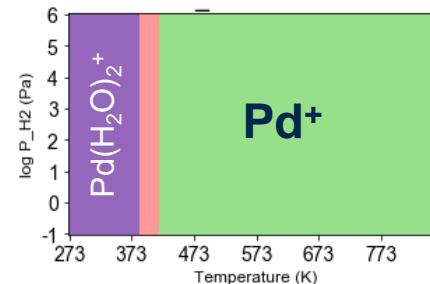
Isolated Al



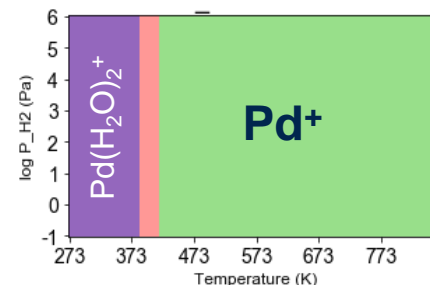
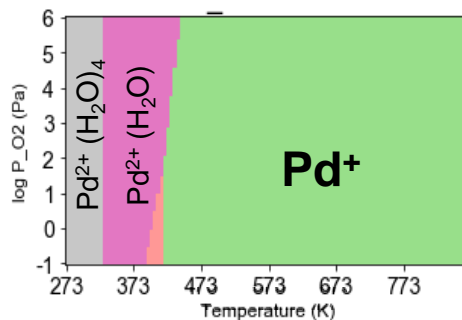
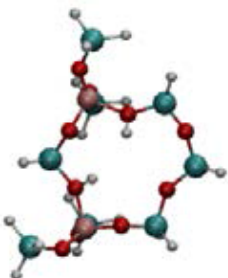
wet, oxidizing feed



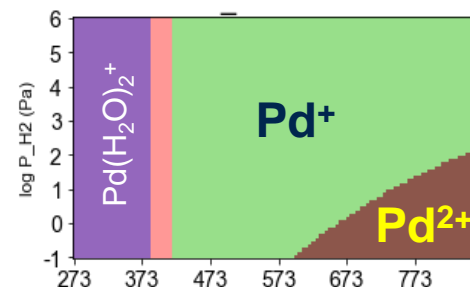
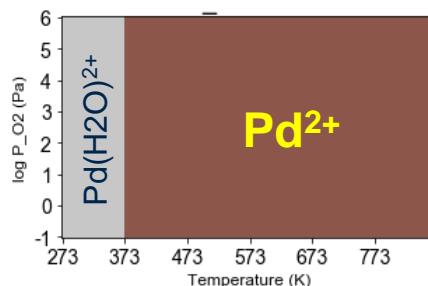
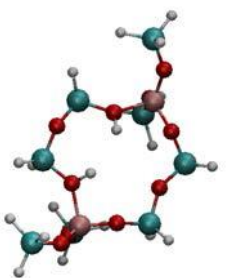
wet, reducing feed



NNN Al pair



NNNN Al pair



Unusual  $\text{Pd}^+$  species is predicted to be most stable over a wide range of oxidizing and reducing conditions

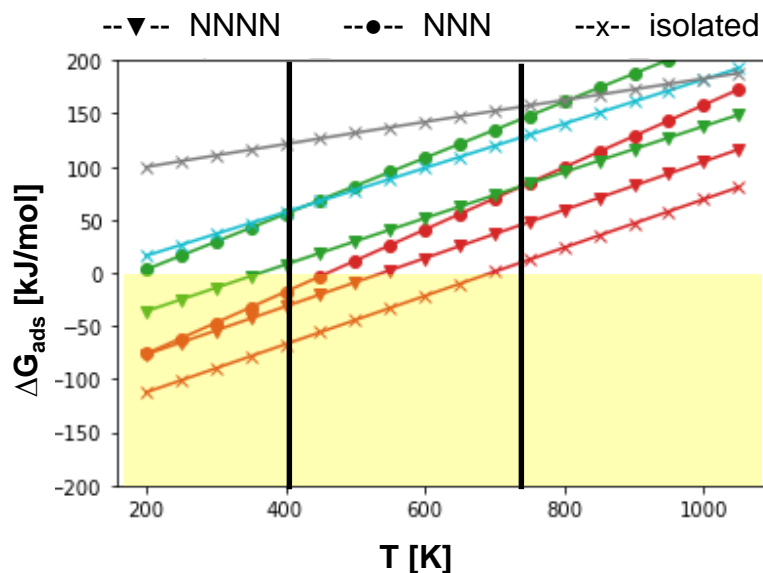


# Computational Study of NO Adsorption

After pretreatment (air + 5% H<sub>2</sub>O; 750 °C),  
Pd<sup>+</sup> at isolated Al and NNN pairs  
Pd<sup>2+</sup> at NNNN pairs

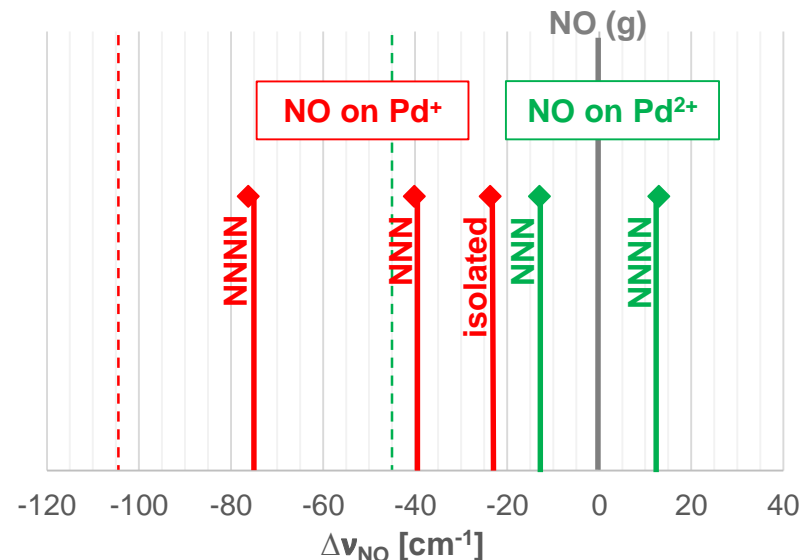
**Does NO adsorb on these sites?**

→  $\Delta G_{\text{ads}}$  ;  $P_{\text{NO}} = 20 \text{ Pa}$



- NO adsorbs on **Pd<sup>+</sup>** (desorption consistent with high T peak in TPD)
- NO does not adsorb on **Pd<sup>2+</sup>**
- NO does not adsorb on **H<sup>+</sup>**

**Additional characterization:**  
**IR stretching frequencies**  
(relative to gaseous NO)



- Calculated NO stretch frequencies vary depending on specific configuration
- NO on Pd<sup>+</sup> stretches appear in region where peaks are observed experimentally (1800 – 1860 cm<sup>-1</sup>)

# Responses to Previous Year Reviewers' Comments

- Project was not reviewed last year

# Remaining Challenges and Barriers

- Understanding the exposure conditions and mechanisms for Pd mobility in zeolites (Pd sintering, Pd re-dispersion, nature of mobile Pd species)
- Identifying the framework Al sites (e.g., proximal or isolated Al) required for stabilizing ion-exchanged Pd
- Identifying the adsorption sites corresponding to different forms of adsorbed NO observed during temperature programmed desorption
- Ascertaining the role – if any – of Pd nanoparticles and PdO clusters, inside CHA cage or on external zeolite surface
- Ascertaining whether Pd<sup>2+</sup> sites undergo partial reduction in situ to enable NO adsorption. Is this facilitated by the presence of CO and/or HC?
- Degradation upon extended cycling is a major barrier to practical implementation

# Future Work

## On-going

- Determine the dependence of ion-exchanged Pd site number and structure on the framework Al arrangement in CHA zeolites
- More accurate calculation of IR features (frequencies + intensities) for comparison with DRIFTS experiments
- In-situ STEM analysis of Pd/zeolites under different catalyst pre-treatment conditions to aid in the interpretation of DRIFTS and XANES spectra
- Effect of CO and HC on NO adsorption: activation of Pd sites through partial reduction (e.g., to Pd<sup>+</sup>) or chemical reaction with NO (e.g., formation of NCO species)?

## Planned

- Explore whether viable reactivation strategies exist for recovering or even preventing catalyst degradation
- Explore how framework type, SAR, Al distribution impact NO<sub>x</sub> storage capacity and durability
- Monolithic Pd/zeolite catalyst performance evaluations in engine exhaust

Any proposed future work is subject to change based on funding levels

# Summary

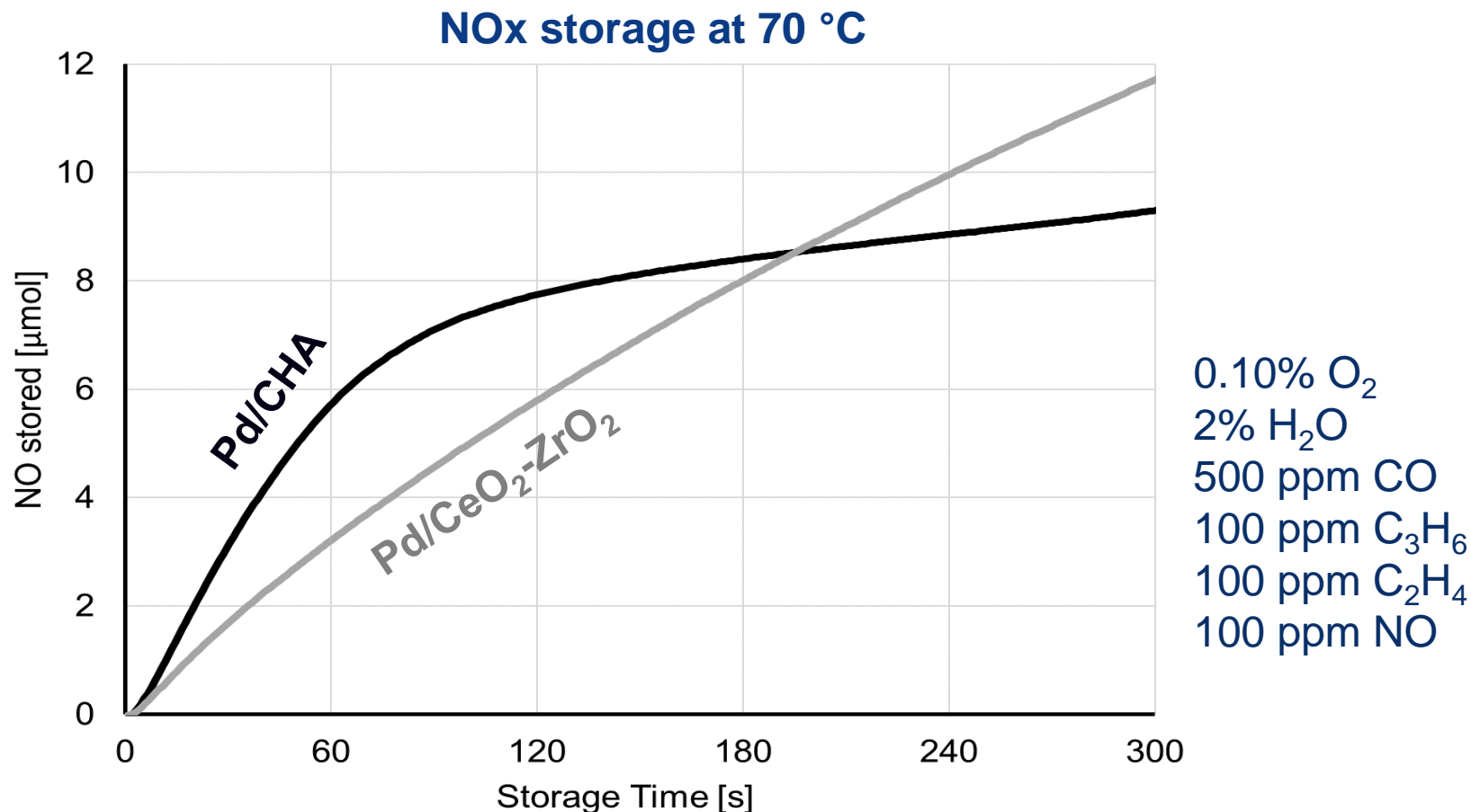
- Quantification of ion-exchanged Pd fraction by different techniques
- Increasing the bulk Al density in the zeolite results in higher amount of sites able to stabilize ion-exchanged Pd species, most likely two proximal aluminum sites
- Isolated  $\text{Pd}^{n+}$  species are essential for NO adsorption, and not metallic Pd/PdO
- Phase diagrams show that ionically dispersed  $\text{Pd}^+$  or  $\text{Pd}^{2+}$  is most thermodynamically preferred under a wide range of conditions
- Stability of  $\text{Pd}^{2+}$  at Al pair sites depends strongly on Al spacing
- $\text{Pd}^+$  is identified as potential high-temperature NO adsorption site,  $\text{Pd}^{2+}$  appears unable to bind NO
- Pd/CHA is more effective for NO<sub>x</sub> storage than Pd/BEA or Pd/CeO<sub>2</sub>-ZrO<sub>2</sub> in both lean (Diesel) and stoichiometric (gasoline) model exhaust feeds
- NO<sub>x</sub> storage on Pd/CHA is almost independent of oxygen level, but storage efficiency and release profile depend on the presence of reducing species
- NO<sub>x</sub> storage is repeatable across several tests, but degrades significantly during extended cycling

# Technical Back-Up Slides

# Milestones for FY2020

| Task  | Date     | FY2020 Milestone Description  | Status     |
|---|----------|---|------------|
| Reactor studies                               | 2/28/20  | Steady state kinetics of NO reduction by C <sub>2</sub> H <sub>4</sub> and CO determined for Pd/CHA and Pd/BEA  | To be done |
| Catalyst characterization                     | 5/31/20  | Structure-property relations between Pd site types, spectroscopic features, and NO/HC adsorption behavior elucidated  | To be done |
| Reactor studies                               | 8/31/20  | Cold start performance of Pd/CHA and Pd/BEA evaluated under simulated stoich. gasoline, lean burn gasoline and diesel exhaust   | To be done |
| Computational studies                         | 11/30/20 | Energy and free energy landscapes for reactions of coadsorbed NO/CO, NO/ C <sub>2</sub> H <sub>4</sub> , & NO/CH <sub>3</sub> C <sub>6</sub> H <sub>5</sub> derived for Pd/CHA and Pd/BEA               | To be done |
| Catalyst aging studies                        | 11/30/20 | Mechanism of Pd/zeolite catalyst degradation under hydrothermal aging elucidated  | To be done |
| Prediction of vehicle performance             | 11/30/20 | Impact of new catalyst on tailpipe emissions estimated using vehicle emission model   | To be done |
| Catalyst performance validation<br>(Go/no-go) | 11/30/20 | Optimized HC/NO adsorber catalyst validated using engine exhaust: NO adsorption and high temperature retention (up to 300 °C) superior to Pd/CeO <sub>2</sub> -ZrO <sub>2</sub> after 50 h 4-mode aging | To be done |

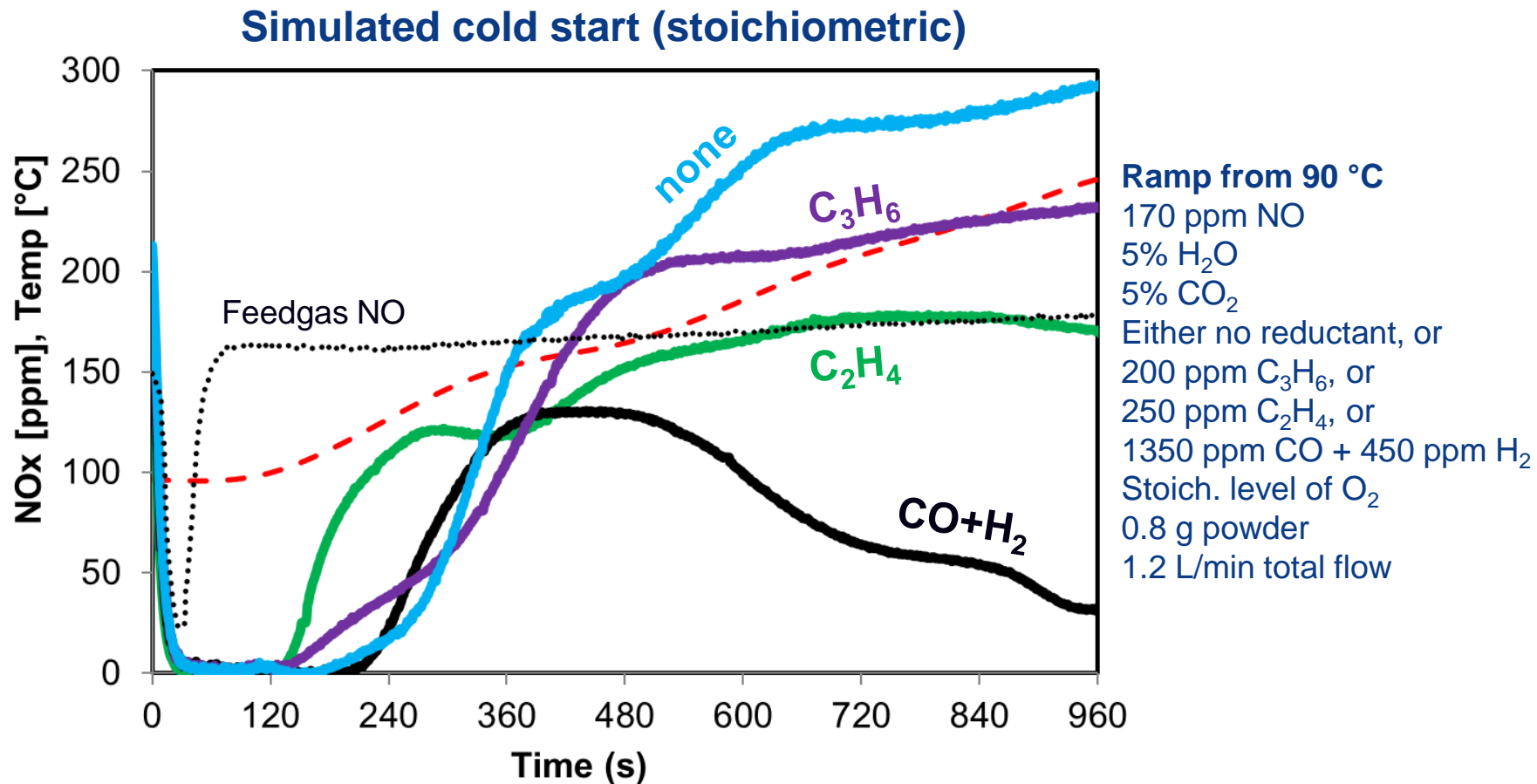
# Comparing PNA Technologies (stoichiometric)



**Initial storage efficiency of Pd/CHA is almost double that of Pd/CeO<sub>2</sub>-ZrO<sub>2</sub>**



# Pd/CHA: Effect of Reductant on NO<sub>x</sub> Storage

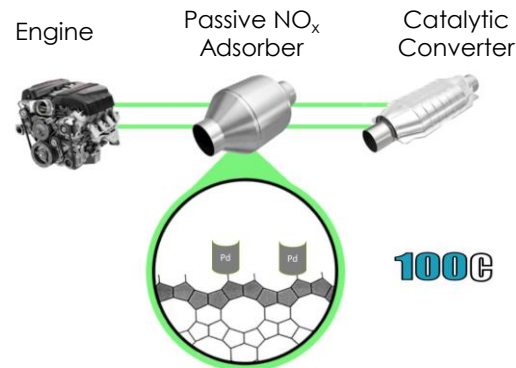


NO<sub>x</sub> storage and conversion highest with CO+H<sub>2</sub>, lowest with C<sub>2</sub>H<sub>4</sub>

# Reactor studies of NO/HC adsorption

## Objective

- Optimize adsorption conditions to achieve high uptake of NO
- Investigate the effects of varying these conditions and other co-feed chemicals (e.g.  $C_2H_4$ , CO, etc.)



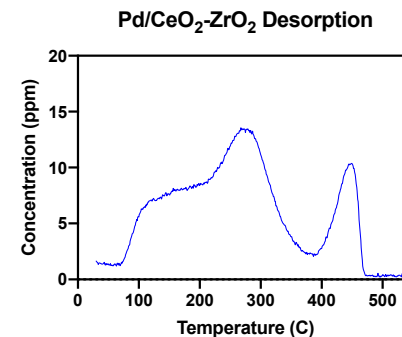
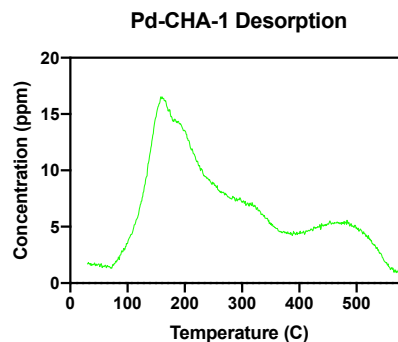
## Methodology

- Pretreatment:** feed air (20%  $O_2$ ) and 5%  $H_2O$ , and heat sample to 750°C for five hours
- Adsorption:** at selected adsorption temperature (typically 75°C), feed ~200 ppm NO in He and 1%  $CH_4$  as tracer
- Desorption:** run temperature-programmed desorption, and heat catalyst to 500°C in He flow at 10°C/min
- Post treatment:** regenerate adsorption sites by flowing a mix of He, air, and  $H_2O$

## Key Findings

Adsorption capacity of Pd-CHA-1 larger than that of PNA standard (Pd/CeO<sub>2</sub>-ZrO<sub>2</sub>) under feed of NO in He

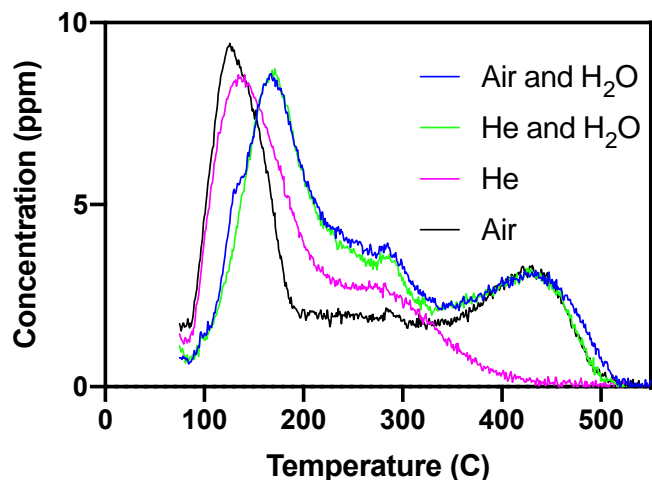
| Catalyst                              | NO/Pd<br>Adsorption | NO/Pd<br>Desorption |
|---------------------------------------|---------------------|---------------------|
| Pd-CHA-1                              | 0.11                | 0.11                |
| Pd/CeO <sub>2</sub> -ZrO <sub>2</sub> | 0.06                | 0.09                |



# Reactor studies of NO/HC adsorption

## Key Findings (continued)

### Desorption - Effect of Post Treatment

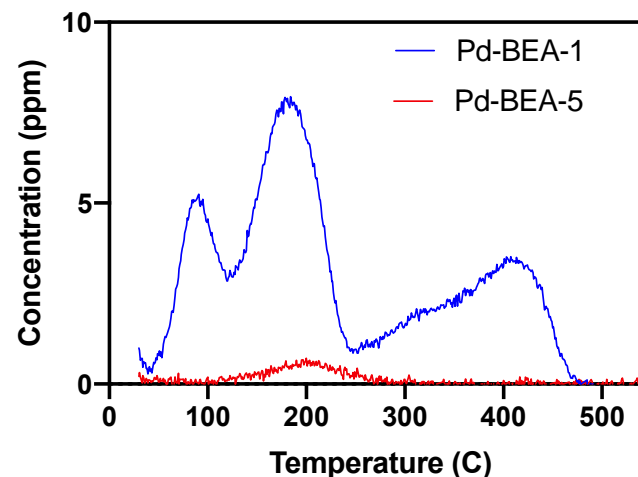


- $O_2$  in air is sufficient to regenerate most NO adsorption sites but  $H_2O$  is essential to fully regenerate the high-temperature sites of Pd-CHA-1.

## Future Steps

Investigate the adsorption of  $C_2H_4$  and the effect of co-feeding on NO adsorption.

### Desorption - Effect of isolated Pd



| Catalyst | NO/Pd      | NO/Pd      |
|----------|------------|------------|
|          | Adsorption | Desorption |
| Pd-BEA-1 | 0.02       | 0.02       |
| Pd-BEA-5 | 0.001      | 0.001      |

- For Pd-BEA-1,  $Pd_{iso}/Pd_{total} = 0.79$  (after 200°C pretreatment). For Pd-BEA-5,  $Pd_{iso}/Pd_{total} = 0.03$ , suggesting that isolated Pd sites are more important for NO adsorption than Pd nanoparticles or PdO clusters.
- Also, the fraction of NO desorbing from the high temperature site (around 400°C) are the same for both the Pd-CHA-1 and Pd-BEA-1 samples – suggests that they share the same site/state of Pd.